# Fugacity and fugacity coefficient excersise

#### **Problem statement**

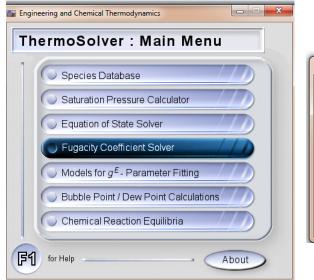
Prepare a graph that shows the change in the fugacity and fugacity coefficient (both in the same graph) when the composition changes for natural gas. Determine the change of the fugacity and fugacity coefficient of natural gas (considering it's a mixture of ethane and propane) at 50 bar and a temperature of 20°C.

## Development

1. We open the *Thermosolver Software*.

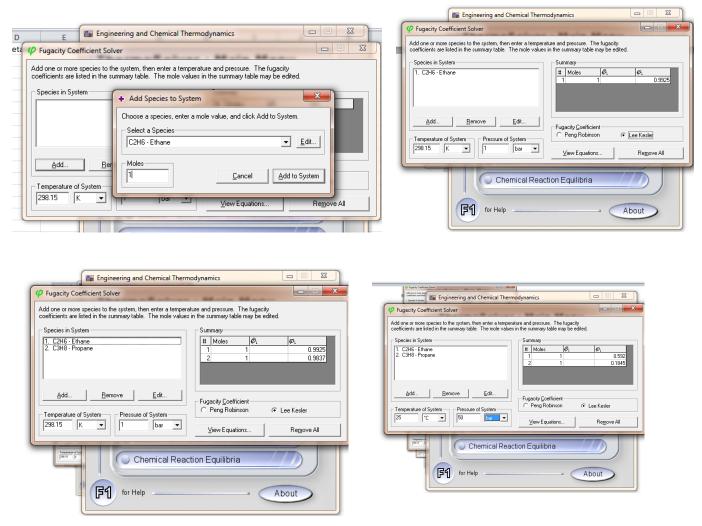


2. We picked the Fugacity Coefficient Solver option.

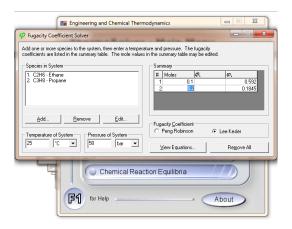


dd one or more species to the system, then enter a temperal coefficients are listed in the summary table. The mole values	
Species in System	- Summary
	# Moles $\hat{\mathscr{O}}_i$ $\mathscr{O}_i$
Add <u>R</u> emove <u>E</u> dit	Fugacity <u>C</u> oefficient © Peng Robinson C Lee Kesler
298.15 K 💌 1 bar 💌	View Equations Remove All

**3.** We add the two components that we are going to use: ethane and propane for 1 mol and we choose Lee Kesler equiaton.



**4.** We observed that if we change the number of moles the fugacity coefficient does not change at all, and this makes sense because these two component are not interacting. This is becasuse we take the statement that the activity coefficient behavies equal in the mixture as is does in the pure state.



**5.** With this two constants:

## **Fugacity coefficient Ethane (Ø):** 0.592

#### **Fugacity coefficient Propane: (Ø)** 0.1845

We could create the graph.

$$f = y * \emptyset * P$$

So fist we calculate  $y * \emptyset$ , from 0 to 1 moles.

$$\emptyset = (x_{ethane} * \emptyset_{ethane}) + (x_{propane} * \emptyset_{propane})$$

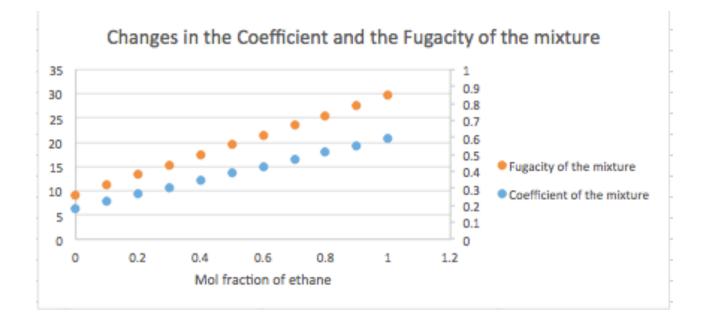
For example:

 $\emptyset = (0.1*0.592) + (0.9*0.1845)$ , then (0.2\*0.592) + (0.8\*0.1845)...

Always with the fugacity coefficients constant.

Then we multiply all the expression by P (50 bar) and so we obtain the fugacity.

	131 🛟 😣	$\bigcirc$ ( $\bigcirc$ fx						
4	A	В	С	D	E	F	G	H
1	Mol fraction of ethane	Coefficient of ethane	Mol fraction of propane		Coefficient of the mixture			Temperatura (°C) 🛛 💌
2	C		1	0.1845				25
3	0.1		0.9	0.1845		11.2625		
4	0.2		0.8	0.1845		13.3		
5	0.3		0.7	0.1845		15.3375		
6	0.4		0.6	0.1845		17.375		
8	0.5		0.4	0.1845		21.45		
9	0.8		0.4	0.1845		23.4875		
10	0.8		0.2	0.1845		25.525		
11	0.9		0.1	0.1845		27.5625		
12	1		0	0.1845		29.6		
13								
14								
15		Changes in the Co	efficient and the Fugacity of	the mixture				
16	3							- • ×
17	30		- 0.9		Ψ	Fugacity Coefficient Se	olver	
18			0.8		Add one or more species to the coefficients are listed in the sum	system, then enter a temperature and pre- mary table. The mole values in the summ	ssure. The fugacity ary table may be edited.	
19	2		0.7		Species in System	Summar		
20	20	•	0.5		1. C2H6 - Ethane	# Mo		Ø,
21	1	5	- 0.4	Fugacity of the mixture	2. C3H8 - Propane	1	0.2	0.592
22 23	10	D 🚽 🕴 🔹 🔍 👘		Coefficient of the mixture		2	0.8	0.1845
23		5	- 0.2					
24	0				Add Bernov	ve Edt		
26						- Fugacity	Coefficient Robinson @ Lee	e Kesler
27						Pressure of System		
28					25 10 •	50 bar 💌 View	Equations	Remove All
29		Pure Ethane	Ethane in the mixture					
30	Fugacity Coefficient	0.5998	0.592					
31	Fugacity (bar)	29.99	29.6					
32								



# 6. Conclusions

Activity coefficient for mixture	Fugacity for mixture	Deviation from ideality
0.1845	9.225	0.8155

0.22525	11.2625	0.77475
0.266	13.3	0.734
0.30675	15.3375	0.69325
0.3475	17.375	0.6525
0.38825	19.4125	0.61175
0.429	21.45	0.571
0.46975	23.4875	0.53025
0.5105	25.525	0.4895
0.55125	27.5625	0.44875
0.592	29.6	0.408

As we know, the fugacity for an ideal mixture is 1. Taking this into account, we can notice that the deviation from the ideality, obtaining the difference between the fugacity of the mixture and the ideal mixture. The greater is the concentration of ethane, the greater the deviation of the mixture. This is due to the molecular interactions, because we have greater molecular interactions between our components. In addition, the ethane is a compound that presents the greatest deviation to the ideality instead of the propane at 50 bars.